
Uncertainty Quantification in an IGCC Process

Using Polynomial Chaos Expansions

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The Future of Coal Power Plants

- Coal provides half of US electricity
- 'Clean' coal – Integrated gasification combined cycle
- Coal → syngas for higher efficiency, CO₂ sequestration

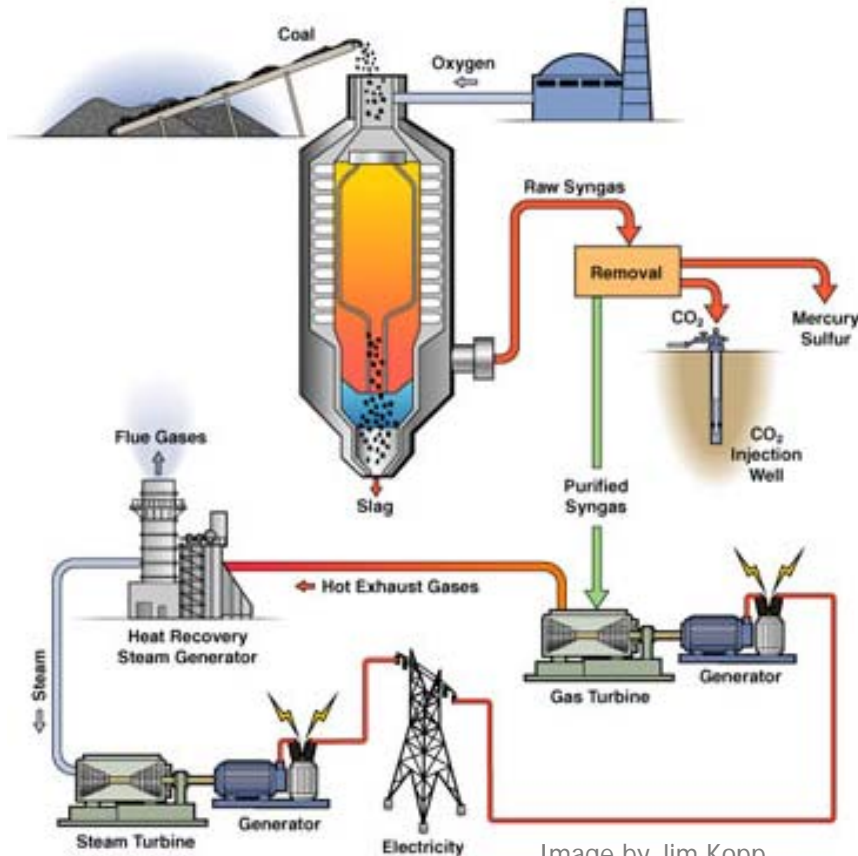


Image by Jim Kopp

Make long term policy & investment decisions

Risk = Uncertainty x consequence

Must quantify uncertainties, especially in complex systems

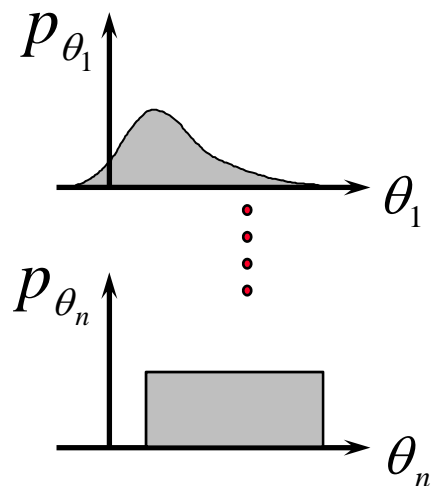
Outline

- Uncertainty Quantification in Chemical Systems
- Tools for Uncertainty Quantification
 - **Polynomial Chaos Expansions**
- Illustrative Examples – Batch reactor
- Coal Conversion Study – Apply to process design
- Future Applications

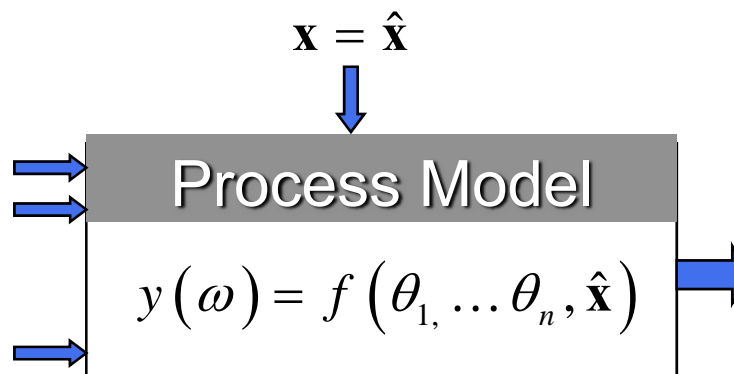
Key Point: The way to get orders of magnitude reduction in solution time is to change the problem **representation** – treat uncertainty at the beginning, not at the end.

Uncertainty Quantification in Chemical Systems

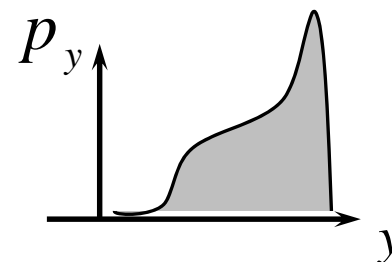
Uncertain Inputs



Independent Variables



Uncertain Output



- Characterize the input uncertainty
- What impact do uncertain inputs have on the outputs?

PDF = probability density function

Not all inputs are Gaussian!

Gaussian inputs  **Gaussian output**

What is the Goal of Uncertainty Quantification?

- **Current Methods – limitations**
 - Perturbation Method – local approximation
 - Moment Methods – linearized systems
 - Monte Carlo – expensive
- **Desired properties of uncertainty methods**
 - Accurate
 - Computationally efficient
 - Decompose output uncertainty ~ Global Sensitivities
 - Apply to nonlinear, black box models
 - Non Gaussian inputs
 - Approximate the full output PDF

Approximation Functions with Expansions

- Fourier Series approximation of functions

$$y(x) \approx \hat{y}(x) = a_0 + \sum_{n=1}^N a_n \sin(nx) + b_n \cos(nx)$$

Basis functions

Coefficients

- Replace an unknown complex function w/ combination of **simple known functions** and **unknown coefficients**

Approximating a Random Variable

- Direct Representation of Random Variables (RV)

$$Y(\omega) \approx \hat{Y}(\omega) = \sum_{j=0}^J y_j \Psi_j(\xi)$$

Basis RVs
↓

Coefficients ↑

Functionals of the Basis RVs ←

- How to choose the best Basis Random Variables and functionals?

Choosing the Basis and Functionals

Recall desired goals:

1. Decompose output uncertainties

How – ensure inputs are independent

Representation – Orthogonal Basis Random Variables

2. Efficient computation of PDF/ statistics

How – Solve multidimensional integrals

$$\text{ex: } E\left[Y(\xi_1 \dots \xi_n)\right] = \int_{\xi_1} \dots \int_{\xi_n} Y(\xi_1 \dots \xi_n) f_{\xi_1 \dots \xi_n} d\xi_1 \dots \xi_n$$

Representation – Orthogonal polynomial functionals

$$\text{ex: } E\left[Y(\xi_1 \dots \xi_n)\right] = \prod_{i=1}^n \left[\int_{\xi_i} Y_i(\xi_i) f_{\xi_i} d\xi_i \right]$$

Expansion of a Known Random Variable

$$X \sim \text{logn}(1, 1/2) \quad \rightarrow \quad X(\omega) \approx \hat{X}(\omega) = \sum_{k=0}^K x_k \Psi_k(\xi)$$

Choose a **Basis RV**

$$\xi \sim N(0,1)$$

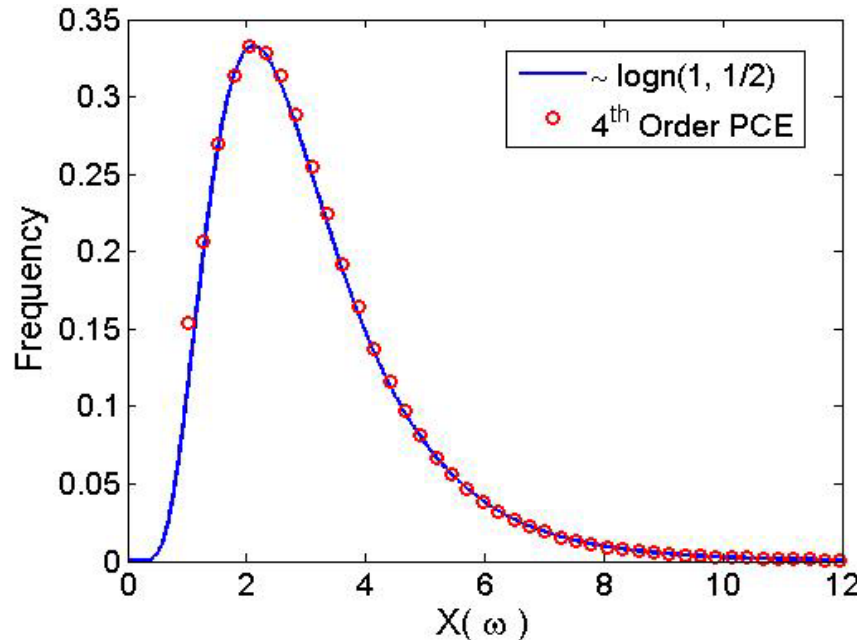
Gaussian Basis RV \rightarrow
Hermite orthogonal polynomials

$$X(\omega) \approx x_0 + x_1 \xi + x_2 (\xi^2 - 1) + x_3 (\xi^3 - 3\xi) + x_4 (\xi^4 - 6\xi^2 + 3)$$

Specify

x =

$$\begin{bmatrix} 3.080 \\ -1.527 \\ 0.392 \\ -0.0597 \\ 0.0117 \end{bmatrix}$$



Algorithm

$$Y(\omega) = \mathcal{A}[X(\omega)]$$

$$X(\omega) \approx \hat{X}(\omega) = \sum_{k=0}^K x_k \Psi_k(\xi)$$

SAME Basis RV!

$$Y(\omega) \approx \hat{Y}(\mathbf{y}, \omega) = \sum_{j=0}^J y_j \Psi_j(\xi)$$

$$R(\mathbf{y}, \xi) = \mathcal{A}[\hat{X}(\xi)] - \hat{Y}(\mathbf{y}, \xi)$$

$$\int_{\xi_1} \dots \int_{\xi_n} [R(\mathbf{y}, \xi) w_l(\xi)] d\xi_1 \dots d\xi_n = 0$$

$l \in 1 \dots J$

Use Galerkin Projection or **Collocation**
→ Get output PDF

Compare to lower order expansion

Represent Known Inputs

Represent Unknown Outputs

Calculate Residual

Solve for Output Coefficients

Test Expansion Convergence

Done

Increase Expansion Order

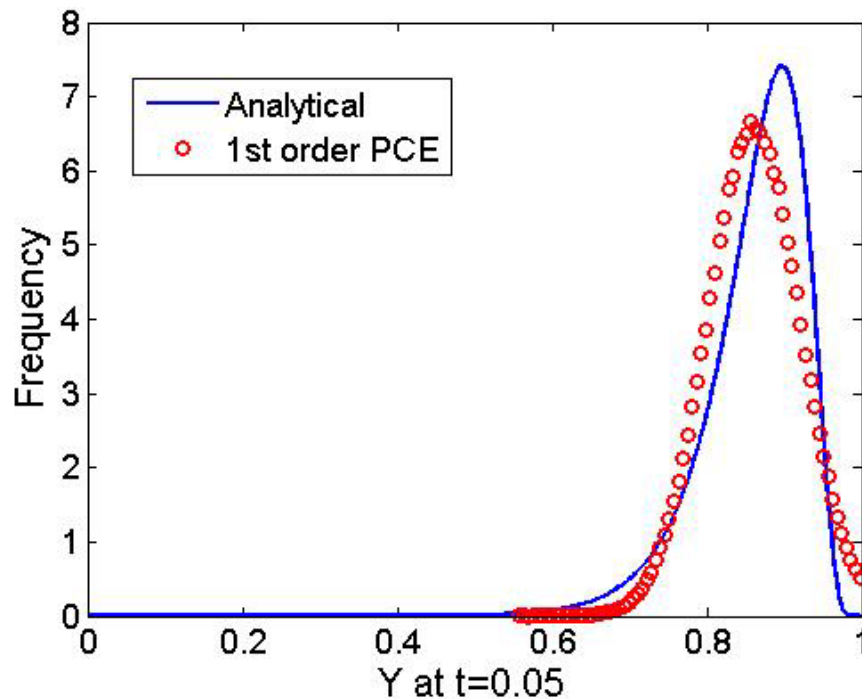
UQ Example – Batch Reactor

$$\frac{dY}{dt} = -X(\omega)Y \quad Y(t=0) = 1$$

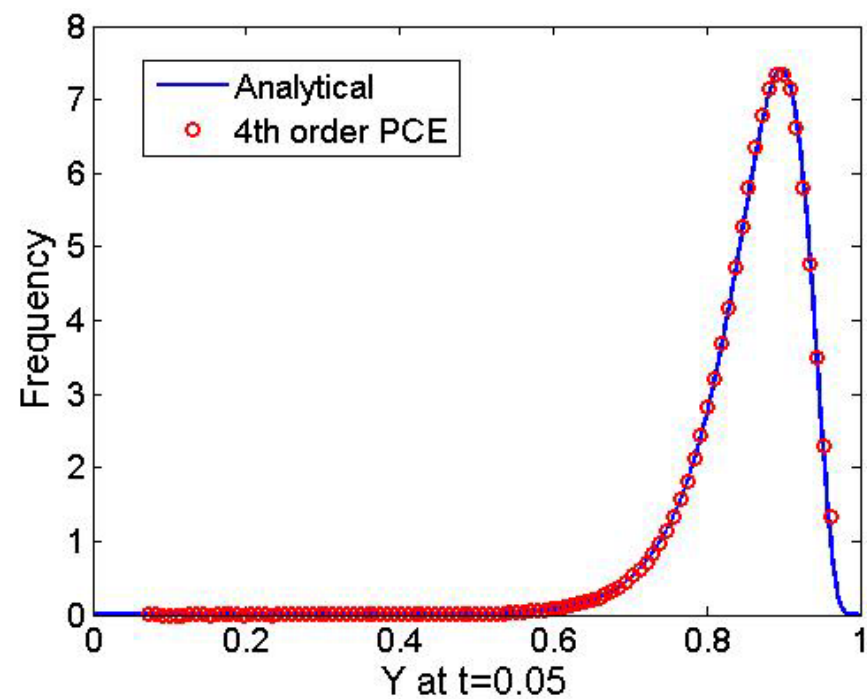
Uncertain kinetic parameter
 $X \sim \text{logn}(1, \frac{1}{2})$

$$Y(t, \omega) = \mathcal{A}[X(\omega)] = \exp(-X(\omega)t) \quad \text{fix } t = \frac{1}{20}$$

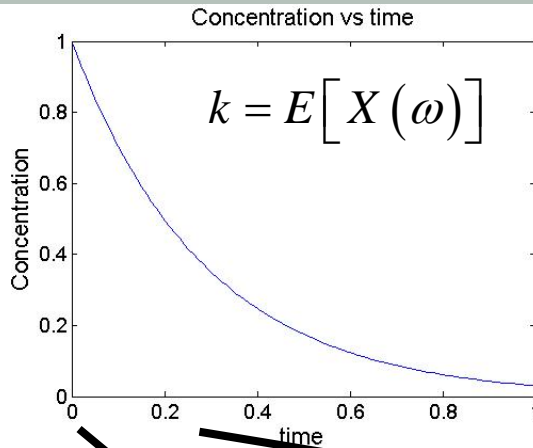
2 model evaluations



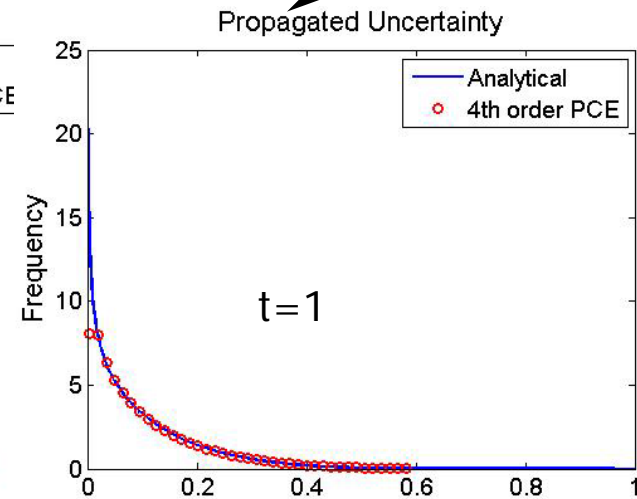
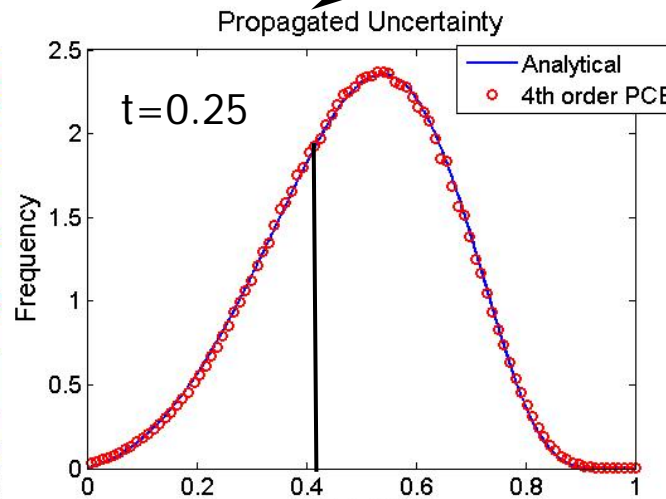
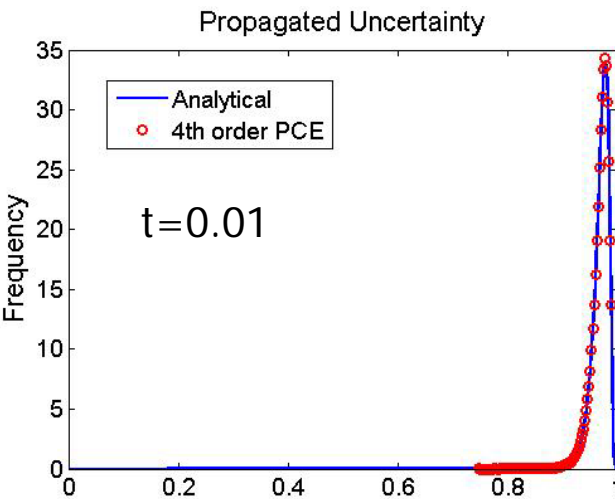
5 model evaluations



Efficient Quantification of Uncertainty



- Uncertainty quantification adds a crucial dimension to the output
- Polynomial Chaos Expansions → 'Probability response surface'



Mean parameter value cannot accurately predict the outcomes

Polynomial Chaos Expansions – Summary

- **Recap**
 - **Widely applicable tool for uncertainty quantification**
 - **Orders of magnitude faster** than Monte Carlo
 - **Easily identify significant input uncertainties**
- **Assumptions/ Issues**
 - **Assume the approximate functional form of the output density**
 - **Requires well behaved models**
 - **Uses concepts from numerical quadrature**
 - **Convergence rate**

Characterize Uncertain Input Parameters

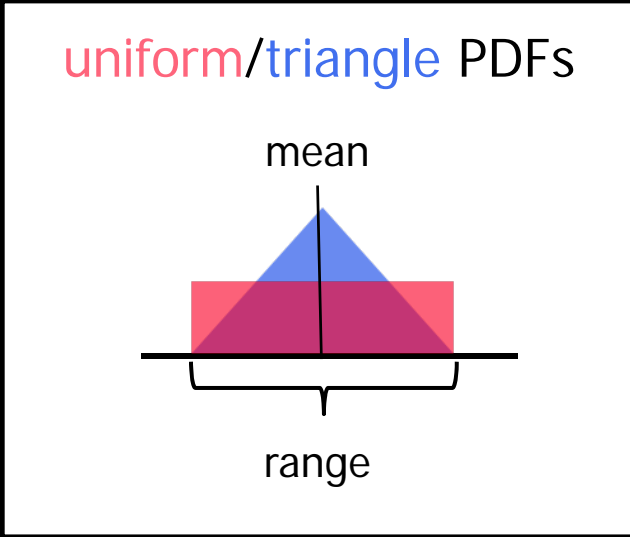
#	Unit	Parameter	Distribution	Mean	Var	Range	σ/μ
1	Feedstock	Moisture	Normal	11.12	0.56		0.067
2		ash	Normal	10.91	0.55		0.068
3		Carbon	Normal	71.72	3.59		0.026
4		Hydrogen	Normal	5.06	0.25		0.099
5		Nitrogen					0.188
6		Sulfur	Normal	2.92	0.14		0.133
7		Oxygen	constrained by other components				
8	Gasification	radiant temperature	Uniform	293	133.33	40	0.019
9		quench temperature	Uniform	210	133.33	40	0.055
10		overall carbon conversion	Triangular	0.980	0.16	0.03	0.40
11	Gas turbine	expander η	Triangular	0.800	0.10	0.1	0.39
12		air compressor η	Triangular	0.850	0.11	0.1	0.39
13		gas turbine isentrop η	Triangular	0.891			
14		gas turbine mech η	Triangular	0.985			
15	Steam turbine	HP-Turbine η	Triangular	0.875	0.12	0.05	0.46
16		MP-Turbine η	Triangular	0.875	0.12	0.05	
17		IP-Turbine η	Triangular	0.895	0.13	0.05	
18		NP-Turbine η	Triangular	0.895	0.13	0.05	
19		LP-Turbine η	Triangular	0.89	0.13	0.05	
20	Air Separation	air compressor η	Triangular	0.804	0.10	0.07	
21		O2 booster η	Triangular	0.735	0.08	0.1	
22		N2 compressor η	Triangular	0.801	0.10	0.07	
23	CO2 Compression	LP compressor η	Triangular	0.850	0.11	0.1	
24		MP compressor η	Triangular	0.850	0.11	0.1	
25		HP compressor η	Triangular	0.850	0.11	0.1	
26		CO2 pump η	Triangular	0.750	0.08	0.1	

21 Parameters

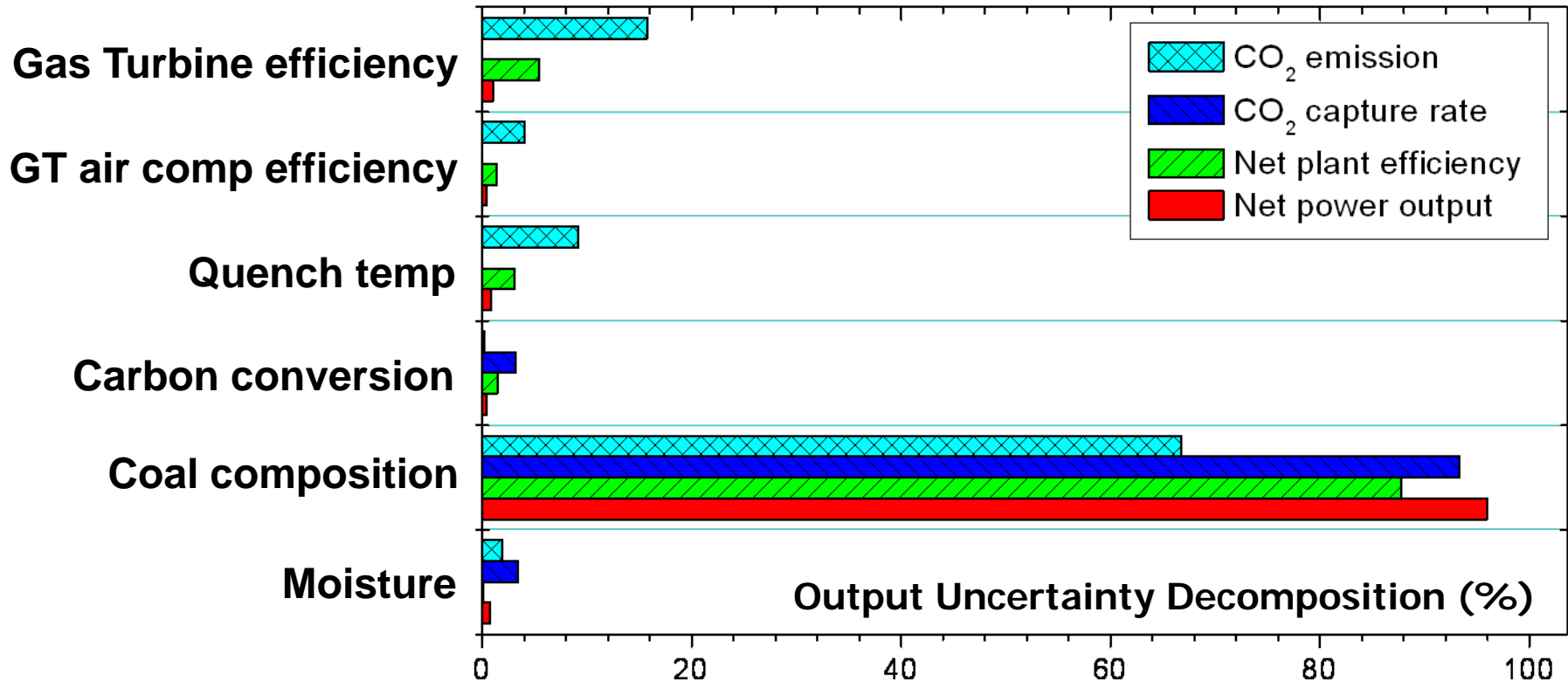
Significant uncertainties

Coal Composition Parameters

Non Gaussian Distributions

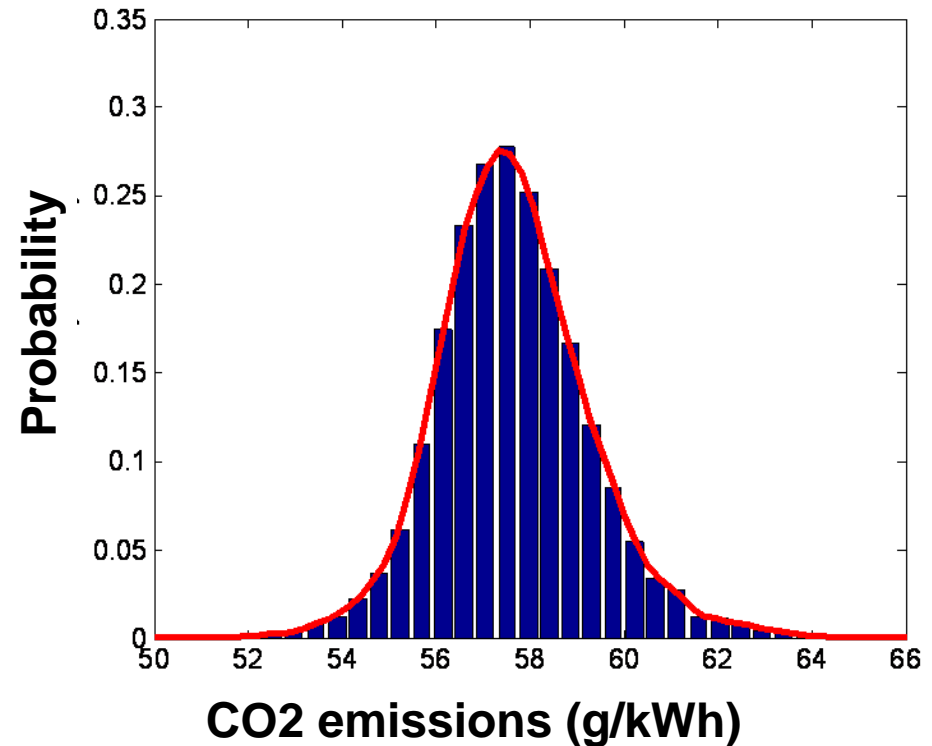
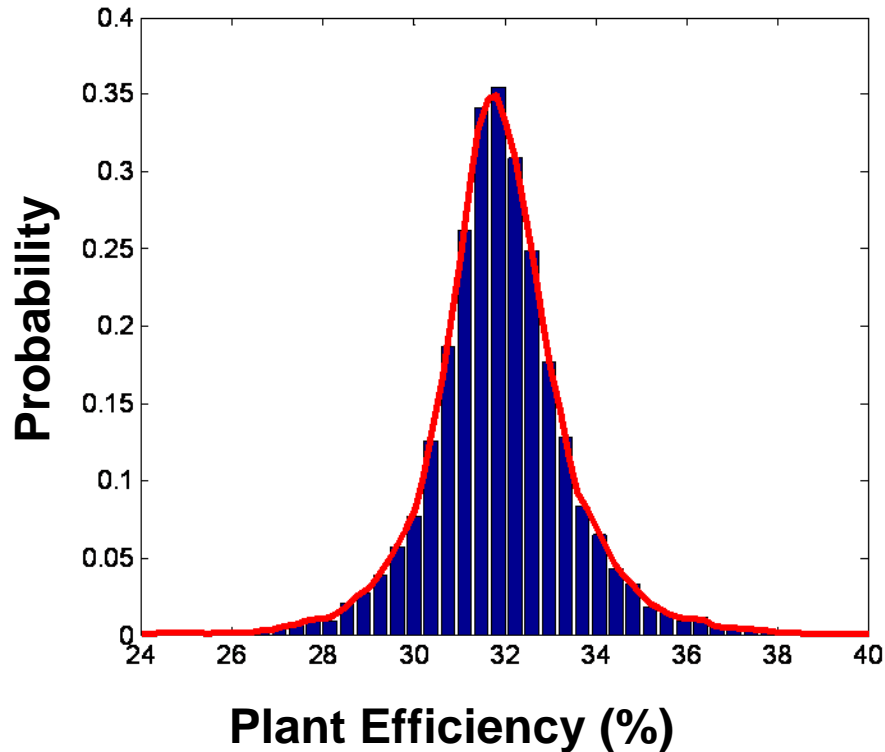


Identify Critical Process Parameters



- Only six parameters have significant impact
- Feedstock is the major factor

Plant Performance Metrics



- **Nearly Gaussian, with significant uncertainties**

Results

- **Model is roughly linear in the significant parameter (Coal composition)**
- **Significant uncertainty in the outputs warrants further study of coal composition, matching of process conditions to coal source.**
- **Efficiency – 48 model evaluations, $\sim O(2)$ fewer than Monte Carlo**
- **Future work – integrate rigorous uncertainty quantification with process design**

Application Areas

- **Current uses**
 - **Computational Fluid Dynamics**
 - **Combustion**
 - **Subsurface flow**
- **Potential Chemical Engineering areas**
 - **Process Design**
 - **Experimental Design**
 - **Economic Analysis**
 - **Model Predictive Control**
 - **Anything related to Stochastic Optimization**

Acknowledgements

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- BP
- McRae Group



References

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